Amendments to the Claims:

This listing of claims below will replace all prior versions, and listings, of claims in the application:

1. (Currently Amended) A process for the preparation and purification of protein(s) ~~using Hydrophobic Interaction Matrix (HIMAX) technology~~ comprising:

(a) lysing, in the absence of a detergent, vector cells expressing said protein(s) to obtain a cell lysate;

(b) centrifuging the cell lysate between 1000g and 10,000g to form a supernatant portion and solid portion;

(c) obtaining the solid portion from step (b) wherein the solid portion comprises the protein(s);

(d) suspending the solid portion in a buffer of pH 6 to [[7. 5]] 7.5;

(e) forming an insoluble matrix after step (d) by the addition of divalent ionic salt having a concentration ranging from 0.2% to 10% with counter ions of either phosphate, chloride and/or acetate solution to the suspension;

(f) subjecting the insoluble matrix to centrifugation ~~optimally~~ to form a pellet;

(g) repeatedly subjecting the pellet from step (f) to a ~~repeated~~ desorption process to release the protein(s) from said insoluble pellet by using either Tris buffer of pH [[8. 0]] 8.0 to 8.5 or Tris buffer with EDTA at pH 7.0 to 8.0; and

(h) recovering the protein(s) through hydrophobic chromatography.

2. (Previously Presented) The process of claim 1 wherein said protein(s) is/are expressed in yeast.

3. (Currently Amended) A process for the preparation and purification of protein(s) ~~by using Hydrophobic Interaction Matrix (HIMAX) technology~~ comprising:

(a) lysing vector cells expressing said protein(s) to obtain a cell lysate;

(b) subjecting the cell lysate to centrifugation ranging from l000g to10,000g ;

(c) obtaining pellet portion from step (b) wherein the pellet portion comprises said proteins;

(d) suspending the pellet portion in a buffer of pH 6 to [[7. 5]] 7.5 having divalent ions ranging from 0.2% to 10% and counter ions of either phosphate, chloride and/or acetate wherein a detergent is not used; and

(e) eluting said protein(s) with Tris ~~base salts of high basicity~~ buffer of pH 8.0 to 8.5.

4. (Previously Presented) The process of claim 2, wherein said protein is a viral antigen.

5. (Canceled)

6. (Currently Amended) The process of claim [[5]] 2, wherein said protein is one other than a viral antigen.

7. (Canceled)

8. (Currently Amended) The process of claim [[7]] 1, wherein the ~~chromotographically~~ chromatographically purified fractions containing the protein(s) are pooled for diafiltration and/or for sterile filtration.

9. (Previously Presented) The process of claim 8, wherein the divalent ionic salt is a salt of divalent cation Zn, Ca, or Mg, or a combination thereof.

10. (Withdrawn) The process as claimed in step (d) of claim 3 wherein the detergent is non-ionic detergent.

11. (Canceled)

12. (Withdrawn) The process as claimed in step (h) of claim 3 wherein ultra filtration is carried out using membrane filters of 100-300K molecular weight cut off.

13. (Withdrawn) The process as claimed in step (h) of claim 3 wherein the ion-exchange matrices is selected from anionic exchange resins such as sulphated cellulose/DEAE matrices.

14. (Previously Presented) The process of claim 8, wherein the said proteins are highly purified without the loss of biological activity.

15. (Currently Amended) The process as claimed in any of the preceding claims wherein contaminants do not interfere with~~/affect~~ the process of preparation and purification of said proteins.

16. (Previously Presented) The process of claim 2, wherein said proteins are viral antigens, recombinant proteins, and/or biotherapeutic proteins.

17. (Original) The process of claim 16, wherein said proteins are simultaneously prepared and purified.

18. (Previously Presented) The process of claim 16, wherein said proteins are selected from the group consisting of: Rabies antigen, Hepatitis A antigen, Hepatitis B antigen, Diptheria toxoid and Tetanus toxoid.